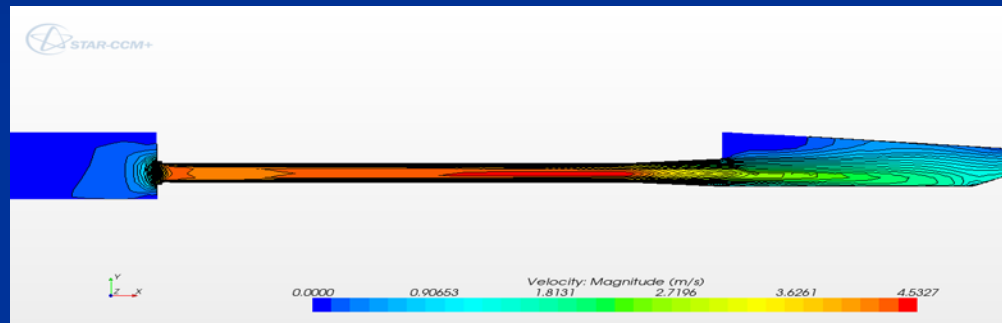


Utilizing Yarnell's Flow Data to Validate & Analyze CFD Models



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Validation of an Outlet Diffuser CFD Model

Initial Concept:

Increase Capacity and Reduce Outlet Losses in Highway Culverts,
Like Draft Tubes in Hydropower

Good Sources of Published Data?

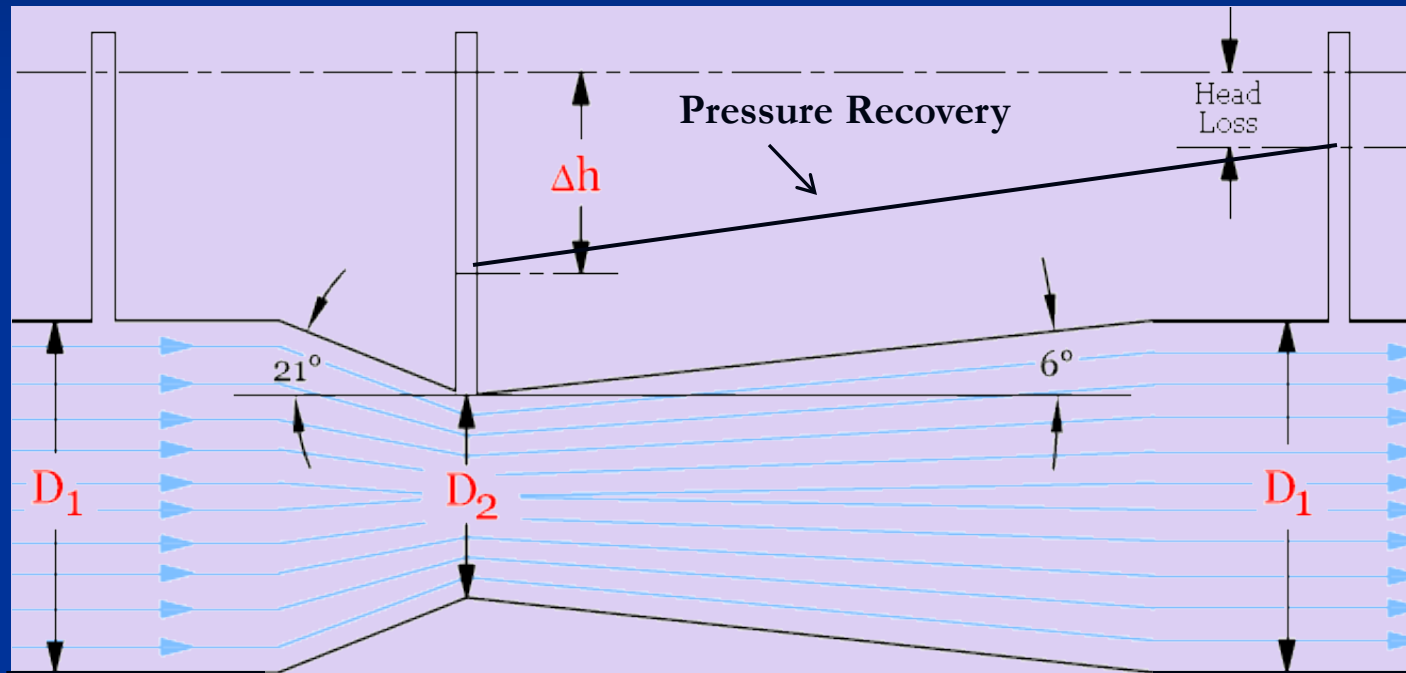
What Concepts Are Involved?

How Would the Available Physical Model Data be Compared to
the CFD Model?

Photo:

Yarnell's 5' long $D = 18''$ to $26''$ Diffuser outlet from his 1926 book
"The Flow of Water Through Culverts"

What is a Diffuser and How Does it Function?



Source: Wermac.org

This Venturi Meter displays the basic concept. 

Yarnell's Model – In this case a 3' by 3' box transitioning into a 6'W by 3'H Outlet Diffuser



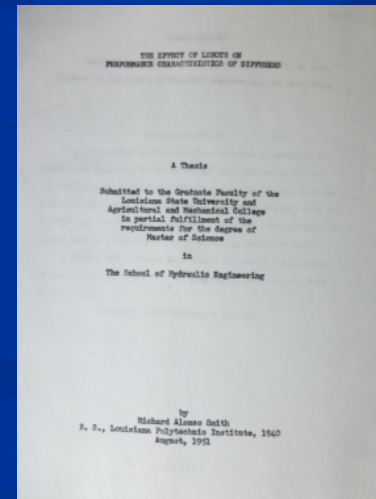
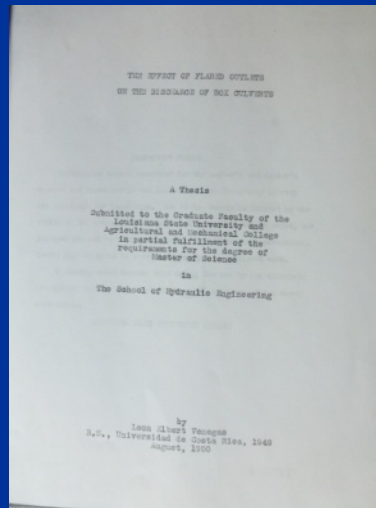
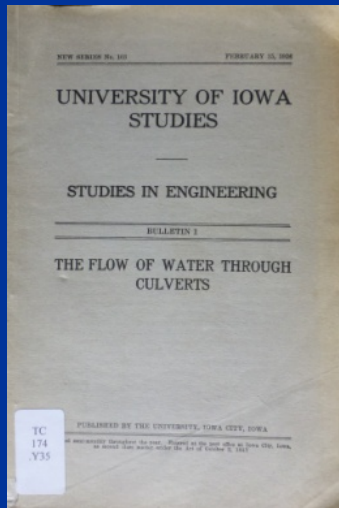
■ Physical Models

- Real Data
- Point Data
- Traditional Sensors _ Piezometers and Pitot Tubes
- Large Physical Presence
- Temporary
- Difficult to Share

Photo curtesy of Connie Mutel, at the University of Iowa Hydraulics Lab

Sources for Physical Diffuser Model Data

- The Flow of Water Through Culverts, Yarnell 1926
 - Pipes, Box Culverts, and Diffusers (“Increasers”)
- Effect of Flared Outlets on Discharge of Box Culverts, Venega 1950
 - Effect of flare angle on discharge of box culverts.
- Effect of Length on Performance Characteristics of Diffusers, Smith 1951
 - Effect of diffuser length on discharge of box culverts.

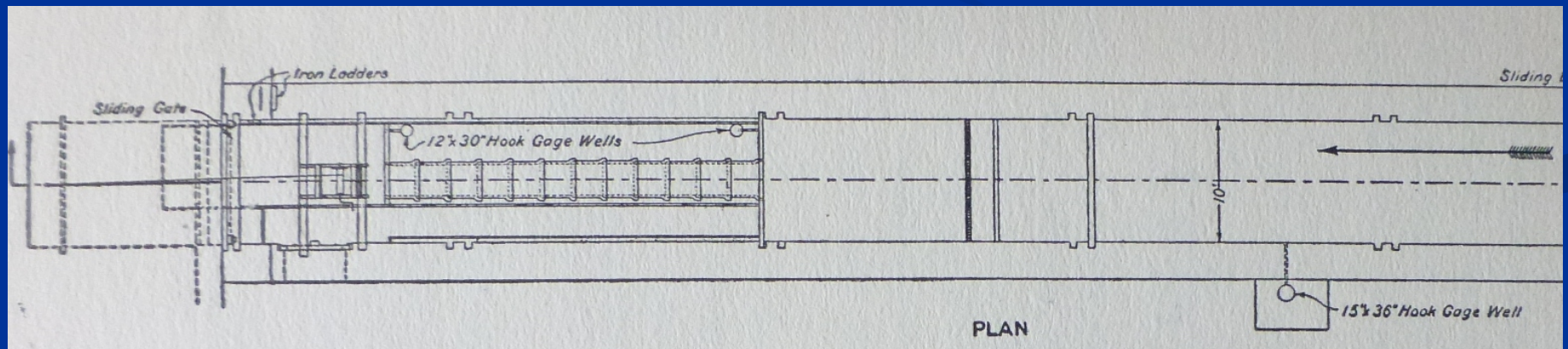


Important Concepts

- Pressure Recovery: Pressure - Velocity Relationship
 - $P_d - P_p = (\rho/2)(V_p^2 - V_d^2)$
- Outlet Losses: Borda-Carnot Derivation (Tullis 2012)
 - $H_o = k_o(V_p - V_d)^2/2g$ where $k_o = (1 - A_p/A_d)^2$
- Effect of Outlet Shape on Pipe Capacity
 - Streamlined Flow:
 - Flume and Syphon Transitions (Hinds 1927)
 - Minimum Energy Culverts (McKay 1971)
- Pipe Roughness and Shear Stress
 - “the action of viscosity ... depends in part on the strength of the force field between the molecules” (Anderson 1998)

Data Management - What is Essential?

- Photos/Images/Detailed Descriptions
 - Essential for model geometry re-creation
- Data Tables
 - Precise but hard to digest
- Plots and Charts
 - Excellent for comparison and summary
 - Not very precise



Yarnell's Data for a Pipe with a Diffuser Outlet

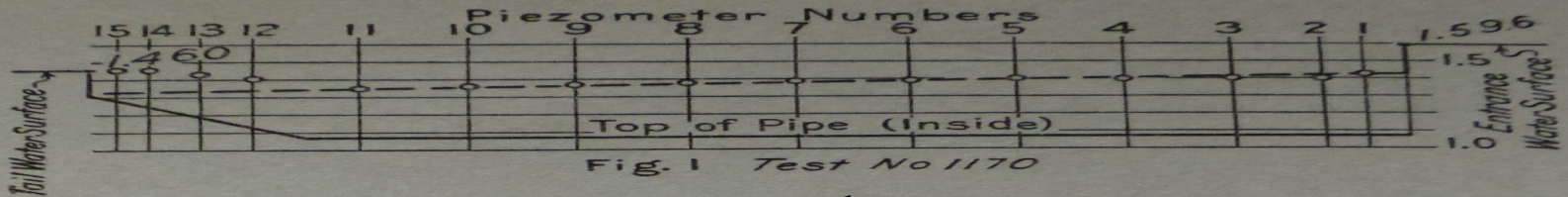
GROUP XI—TABLE 79 SHOWING THE EFFECT OF A CONE PLACED AT THE OUTLET END OF A PIPE CULVERT

Table 79—18-inch vitrified-clay pipe, with straight endwall entrance and without floor in front of pipe; cone, 60 inches long increasing from 18-inches in diameter to 26 inches in diameter, total length of pipe including cone, 30 feet. Area of cross-section, 1.791 square feet; mean hydraulic radius, 0.3775 (See Plate XI-A)

Test numbers	Q Dis-charge Cu. ft. per sec.	V Veloc-ity Feet per sec.	$\frac{V^2}{2g}$ Veloc-ity head	Total head on pipe Feet	Fric-tion loss Feet	En-trance loss Feet	En-trance loss coeffi- cient	Slope	C Chezy coeffi- cient	n Kutter coeffi- cient	n' Man-ning coeffi- cient	Difference in elevation of water surface between entrance and outlet Feet	Gain in head with increaser at outlet Feet	Gain in head divided by velocity head
1167-1169	4.321	2.143	0.071	0.143	0.061	0.011	0.151	0.00199	78.5	0.0153	0.0162	0.07	0.074	1.047
1170-1172	6.02	3.861	0.176	0.264	0.090	-0.002	-0.011	.00292	101.3	.0124	.0125	0.14	0.128	0.729
1173-1175	8.02	4.478	0.312	0.455	0.133	0.010	0.031	.00435	110.9	.0116	.0114	0.24	0.214	0.686
1176-1178	10.05	5.609	0.489	0.747	0.244	0.013	0.027	.00775	103.8	.0122	.0122	0.38	0.363	0.742
1179-1181	12.14	6.778	0.714	1.069	0.339	0.016	0.023	.01104	105.2	.0121	.0120	0.55	0.519	0.726
1182-1184	14.16	7.908	0.972	1.481	0.470	0.039	0.040	.01534	104.2	.0122	.0122	0.74	0.740	0.761
1185-1187	16.50	9.213	1.319	2.011	0.652	0.039	0.030	.02128	103.3	.0123	.0123	1.00	1.015	0.769
1188-1190	18.96	10.59	1.743	2.667	0.876	0.049	0.028	.02856	102.4	.0124	.0124	1.82	1.353	0.777
1191-1192	21.84	12.20	2.312	3.538	1.118	0.108	0.046	.03647	104.0	.0122	.0122	1.76	1.786	0.772

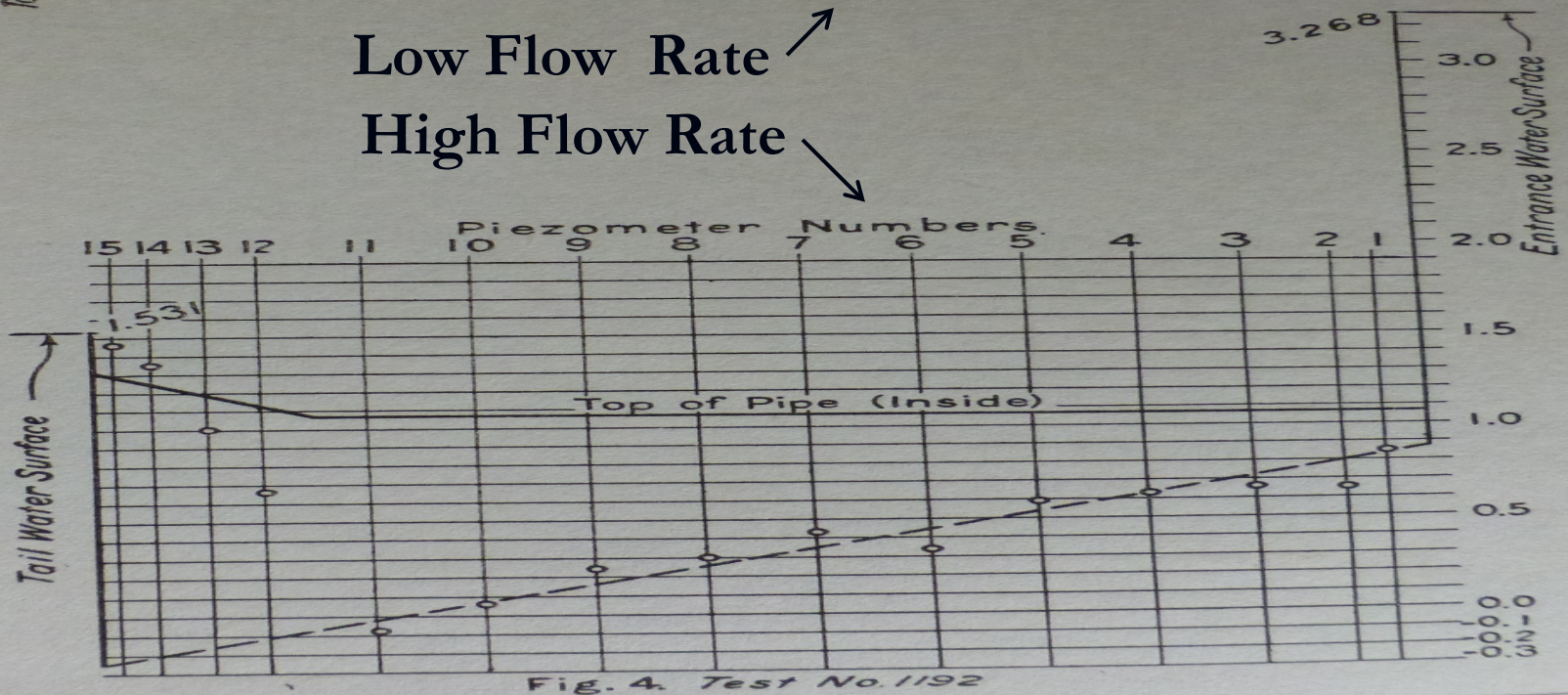
- This data can be converted into a Performance curve.

Yarnell's Diffuser Piezometer Data



Low Flow Rate ↗

High Flow Rate ↘



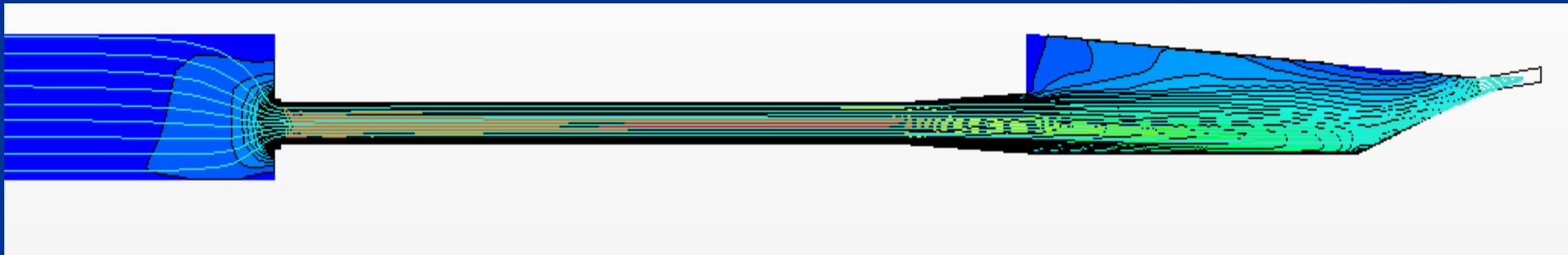
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The addition of this data can be used to create HGL and EGL plots.

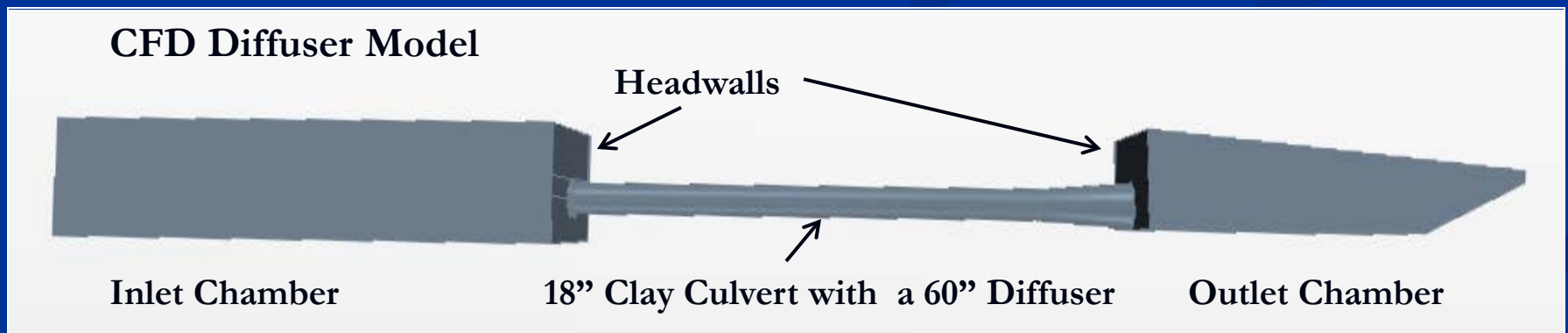
CFD Model Advantages

- CFD Models:
 - Easy to store and share
 - Not limited by physical and cost constraints
- Data and results can be viewed in a number of formats
 - Streamlines and vectors – indicate flow path
 - “Fields” – contoured data indicates gradients
- Data can be combined to display secondary features like shear stress



CFD Models (*cont*)

- Comparison of CFD models with physical models is necessary
 - The CFD program Star-ccm+ handles the basic model well
 - Model differences indicate the need for future research



Insights from CFD Simulation Results

Pressure Profile $Q = 22 \text{ CFS (625 L/s)}$



CFD Replication of Yarnell's Diffuser Model

Pipe Length 30.7', D = 18"

Inlet Chamber

Outlet Chamber

Water Surface

Low Pressure

Water Surface

High Pressure Gradient

Diffuser

Increasing Pressure



78421.

88734.

Absolute Pressure (Pa)

99047.

1.0936e+05

1.1967e+05

1.2999e+05



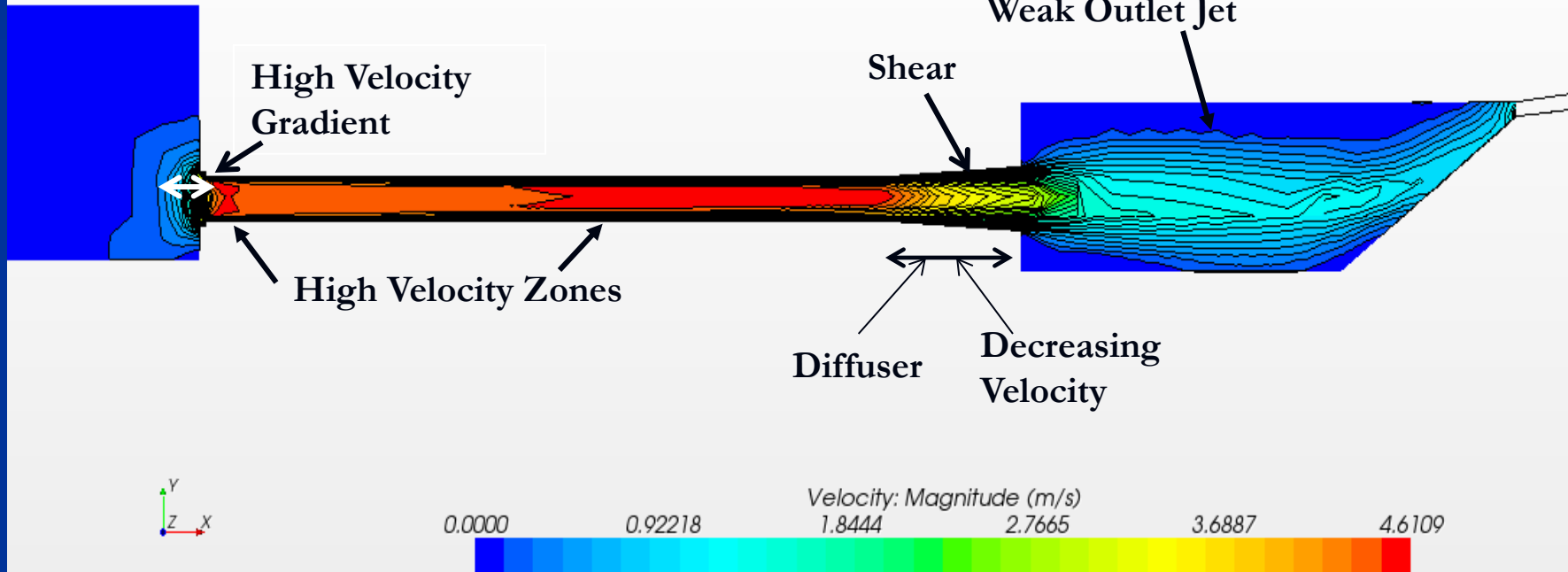
Velocity Profile $Q = 22 \text{ CFS (625 L/s)}$



Inlet Chamber

Pipe Length 30.7', D = 18"

Outlet Chamber



Pressure Profile for a Straight Clay Pipe

$Q = 53 \text{ CFS (1500 L/s)}$

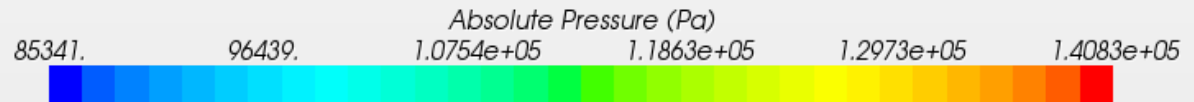
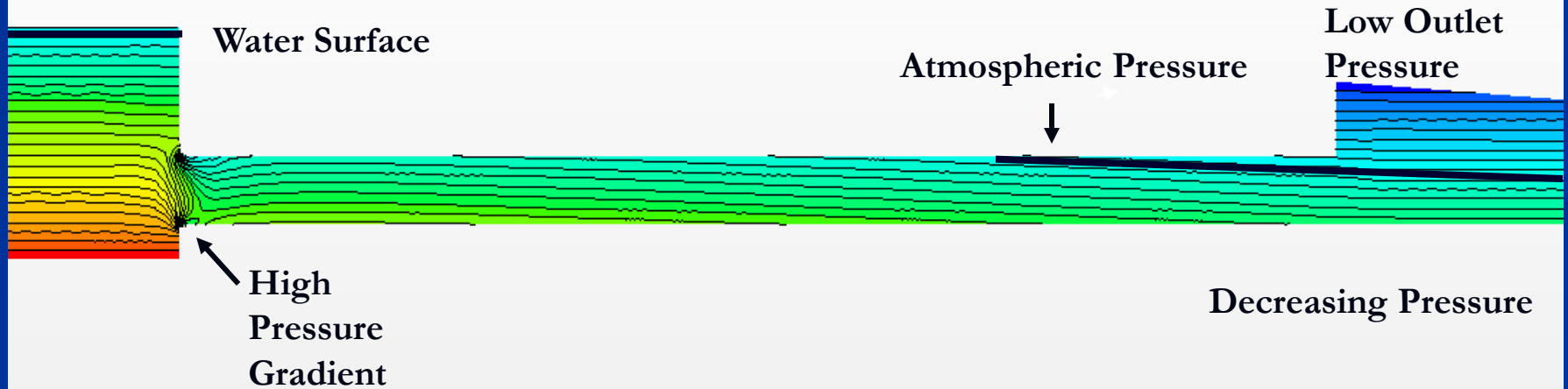


CFD Replication Of Yarnell's 24" Clay Pipe

Inlet Chamber

Pipe Length 38.3', D = 24"

Outlet Chamber



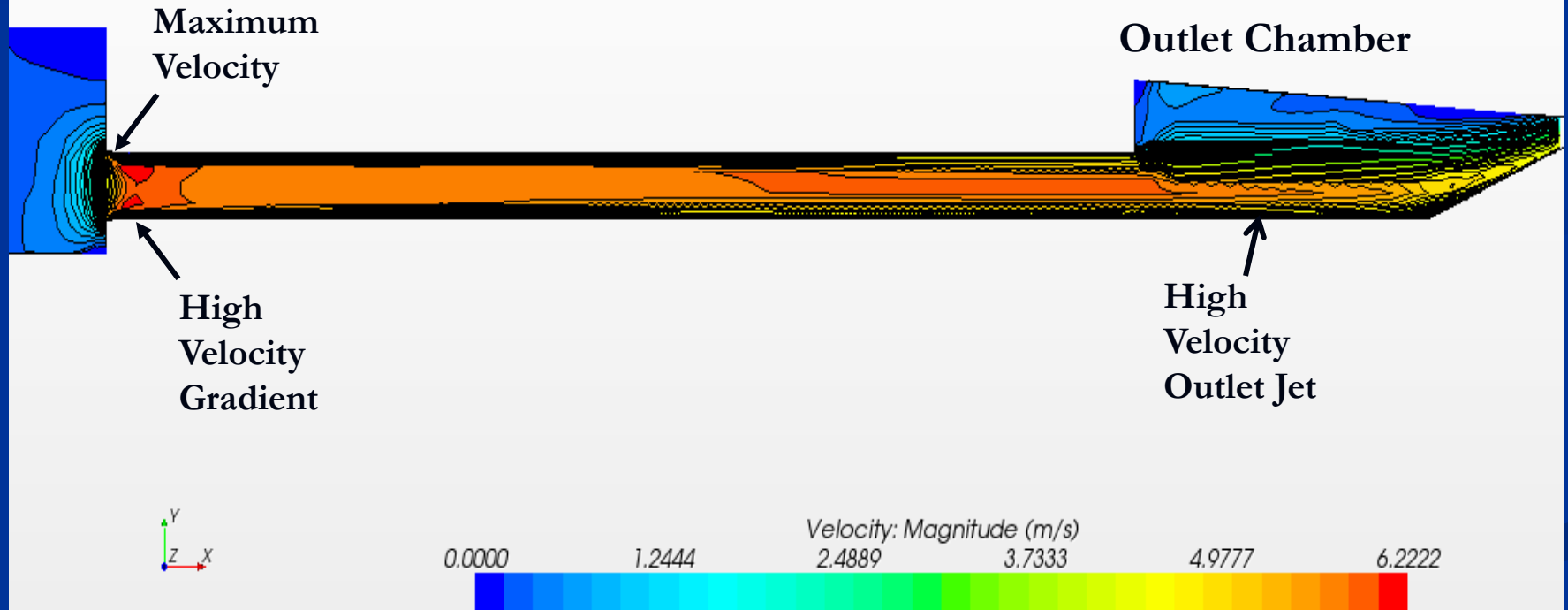
Velocity Profile Straight Clay Pipe

$Q = 53 \text{ CFS (1500 L/s)}$



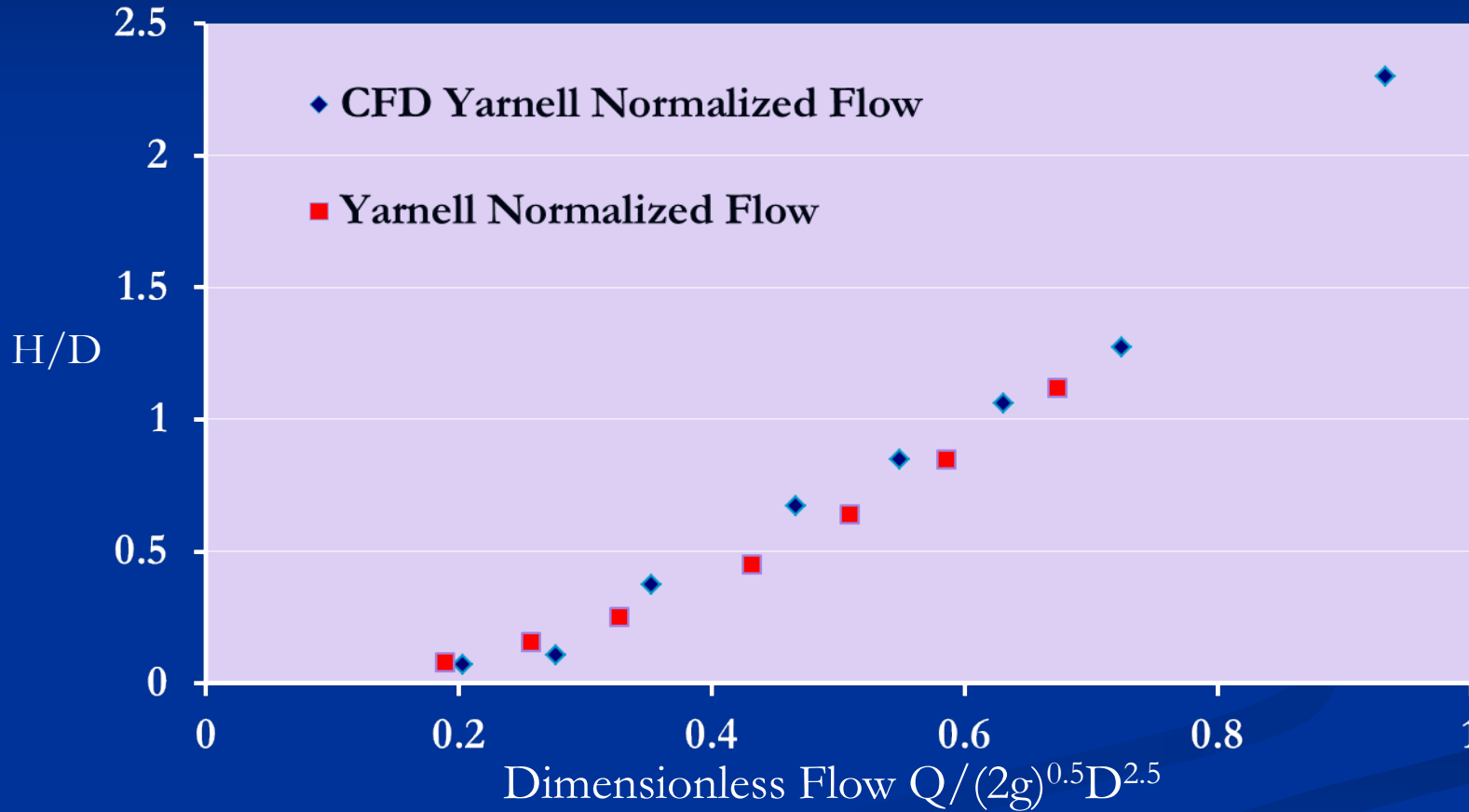
Inlet Chamber

Pipe Length 38.3', D = 24"



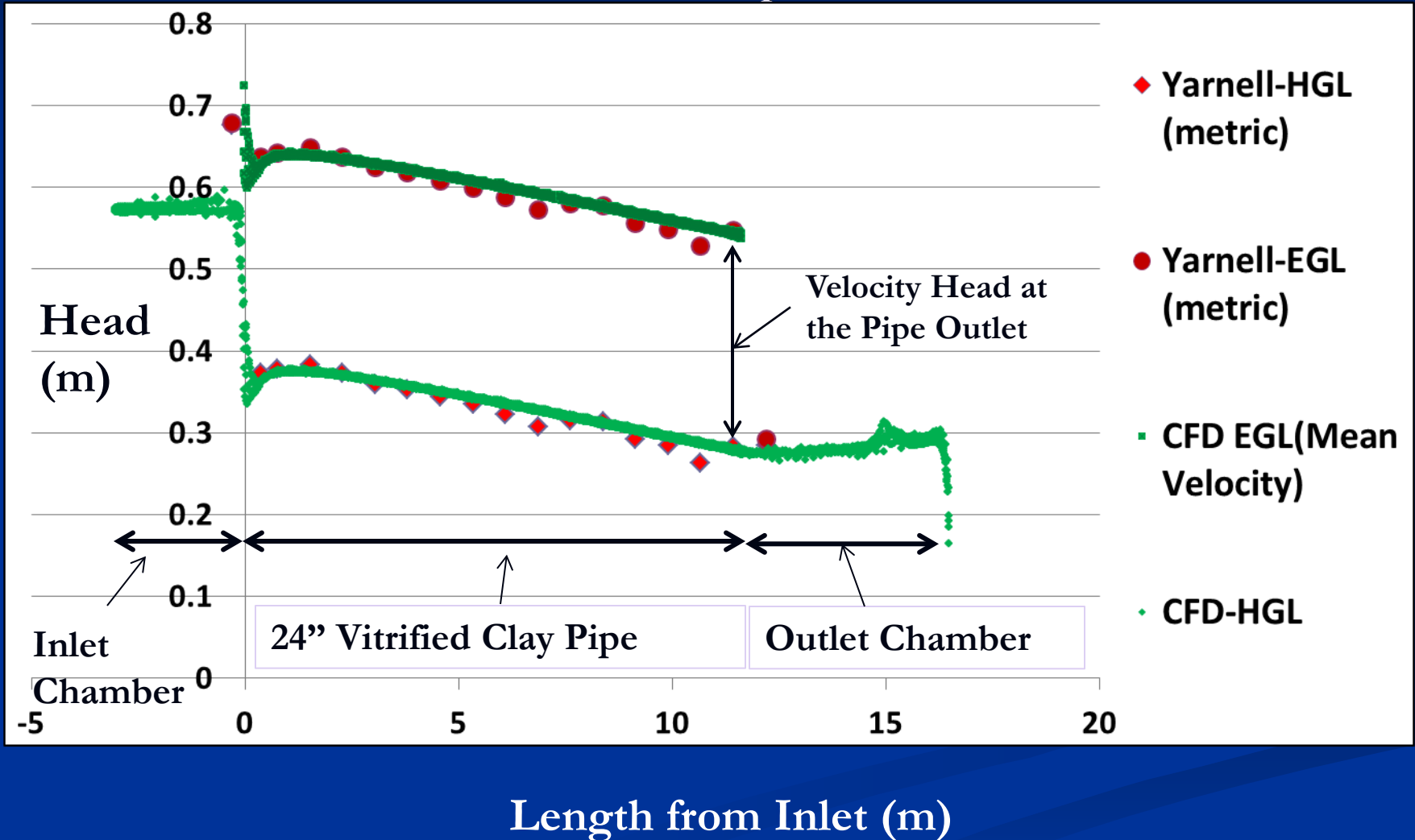
Yarnell & CFD - Performance Curve

D = 24" Clay Pipe Q = 25 CFS – No Diffuser



Yarnell & CFD - HGL & EGL

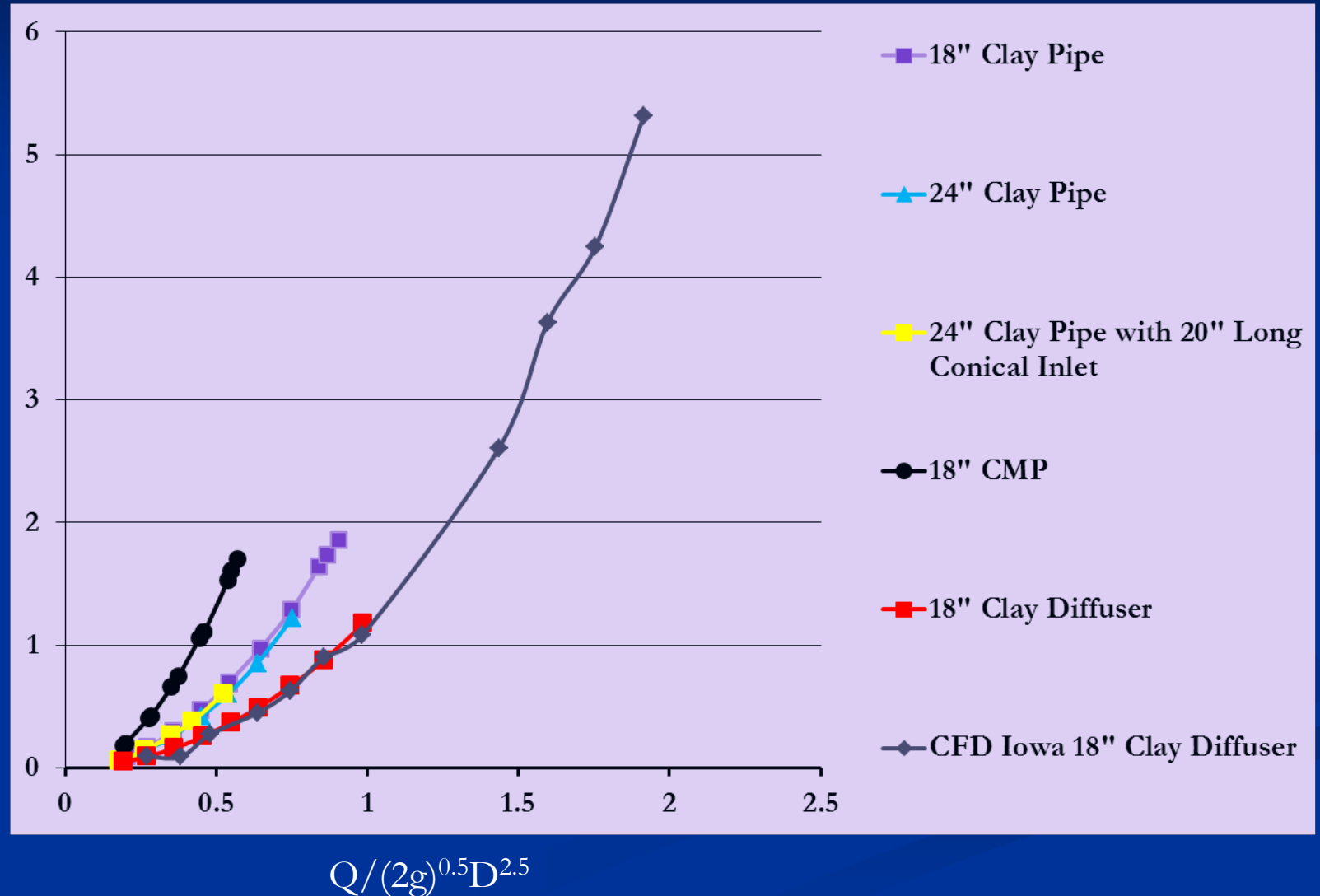
For an 24" Smooth Pipe for 25 CFS



Yarnell & CFD - Performance Curve

D = 18" Clay Pipe with 60"-long diffuser outlet

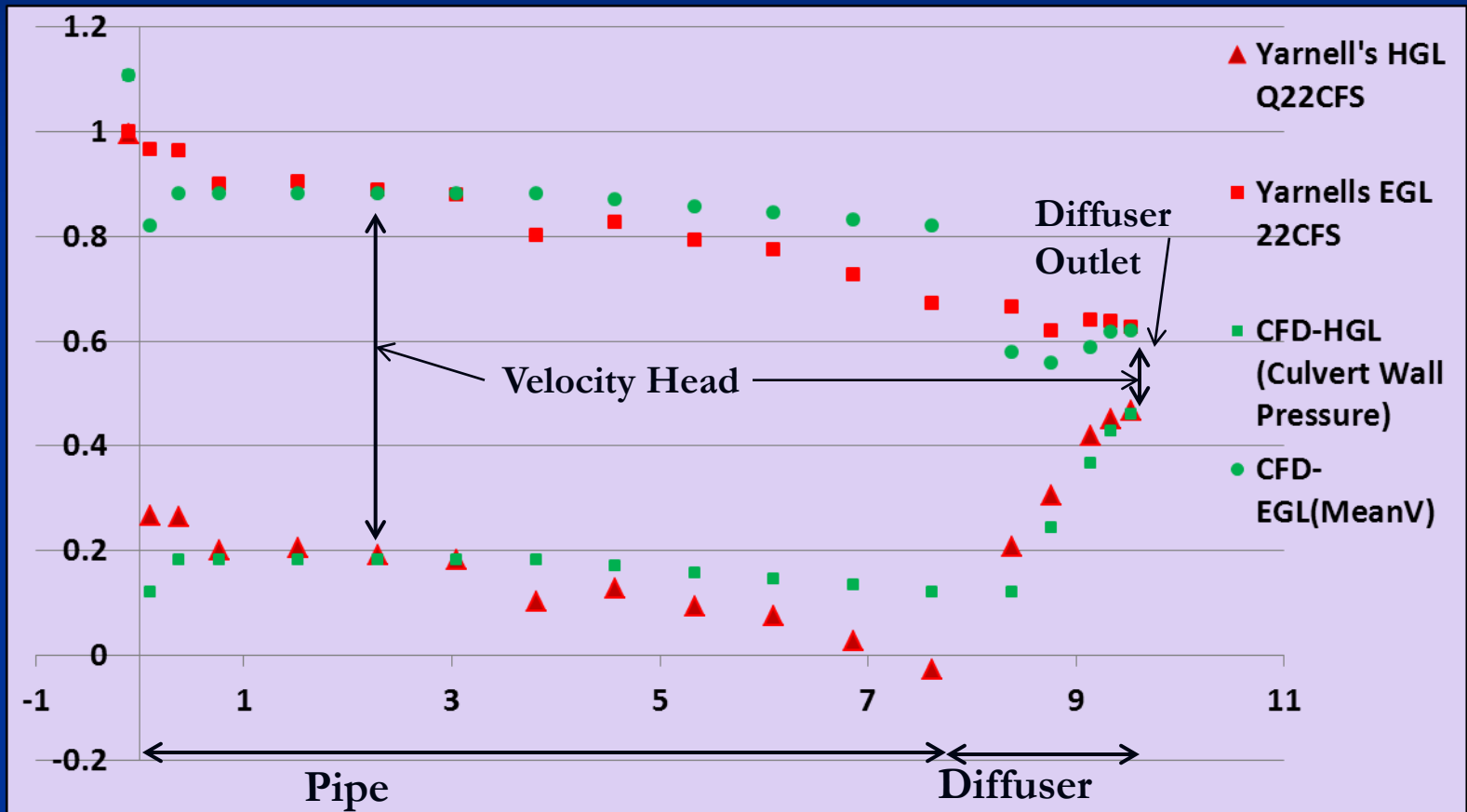
H/D



Yarnell & CFD - HGL & EGL

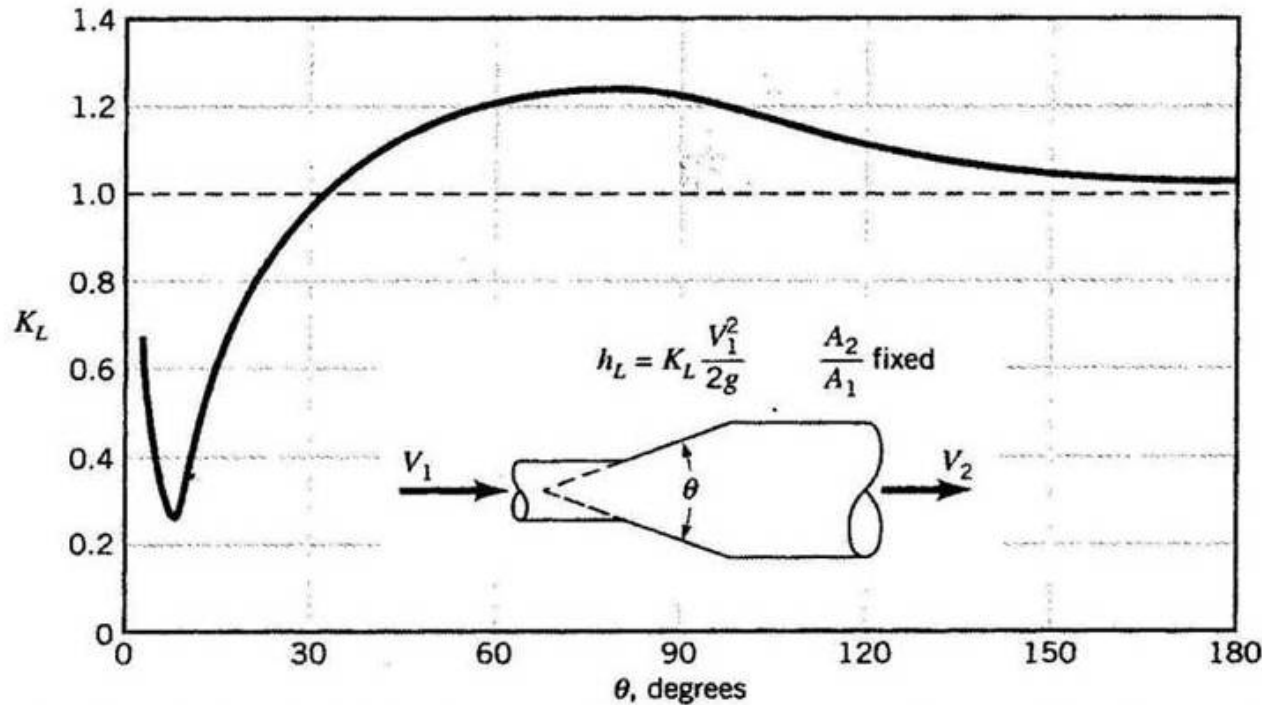
D = 18" Clay Pipe with 60"-long diffuser outlet, Q= 22 CFS

Head
(m)



Length (m)

Outlet Loss Coefficient



■ FIGURE 8.29 Loss coefficient for a typical conical diffuser (Ref. 5).

- Source: Source: Fundamentals of Fluid Mechanics, Munson, Young, p. 502 Okiishi, 1998
- Outlet loss coefficient – Minimized at a flare angle of 12°
- At small flare angles shear with the diffuser wall is the source of the loss
- At large angles separation and recirculation are associated with increased losses

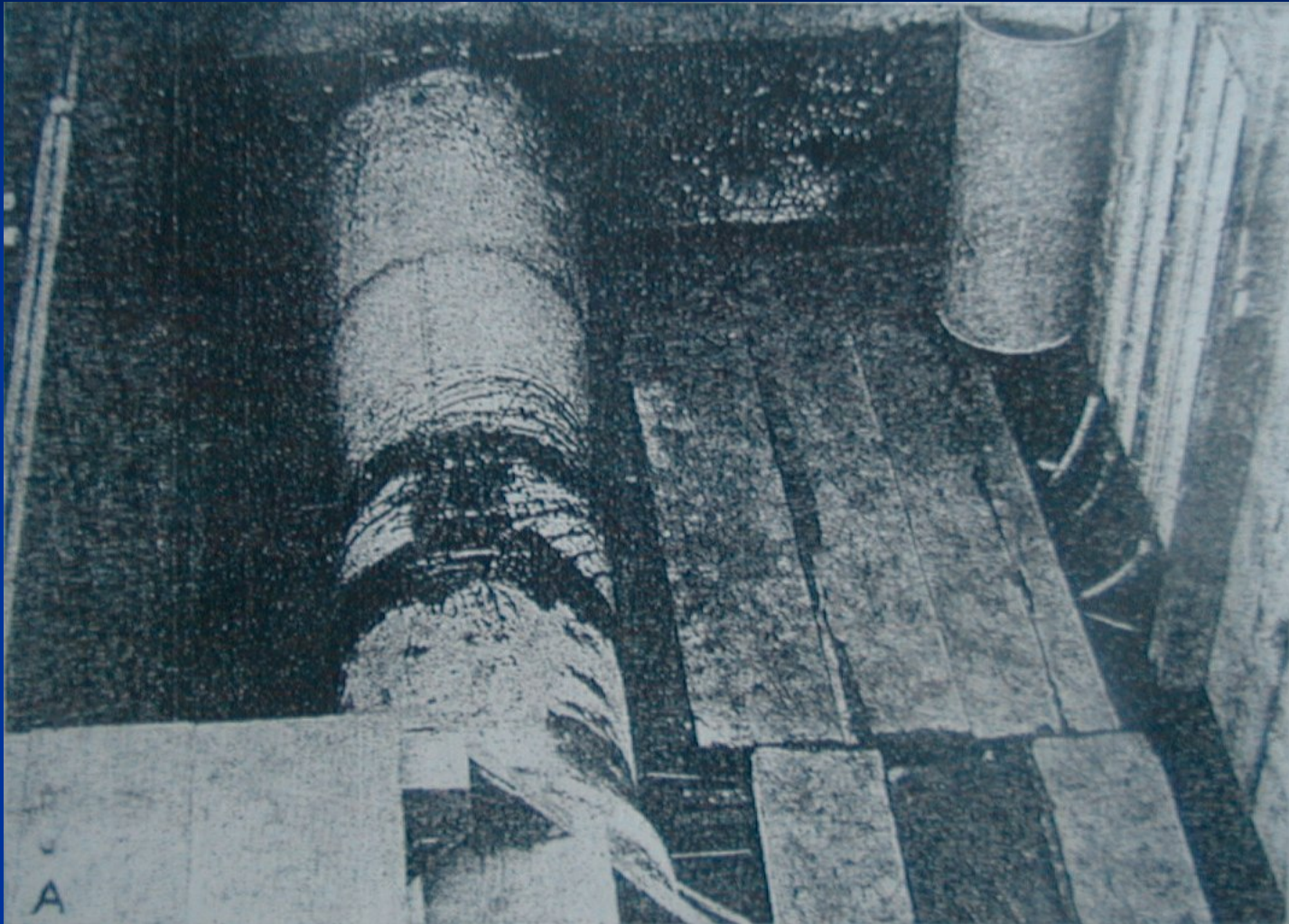
Why the Difference in the Minimum Pressure at the Diffuser Inlet?

- Interaction of water with culvert wall.
 - Pipe Roughness
 - Clay Pipe $n=0.0122$ (roughness height 0.5mm to 1mm)
- Pipe Wall Shear Stress – Rouse's Research
 - “Wetting agents” (hydrophilic)
 - Allow Culvert to fill when $H/D > 0.9$
 - Allow Culvert to stay full to the outlet of the pipe creating a vacuum near the outlet of the pipe.
 - Grease or Wax (hydrophobic)
 - Allow water surface to drop away from the top of the pipe near the outlet loosing the vacuum.

Summary

- By utilizing existing physical model data to calibrate/verify the CFD model many questions can be answered.
- CFD models of simple pipes are relatively easy to construct and the results are very close to physical models.
- Properly designed diffusers function very predictably in both Physical and CFD models.
- The unusual physics of diffusers lead to noticeable differences in the model outputs.

Questions



Yarnell's Diffuser outlet

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